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10533 REFORMER

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=> s feedstock and reformer

26959 FEEDSTOCK

10533 REFORMER

L2 386 FEEDSTOCK AND REFORMER

=> s 12 and wood 205736 WOOD 6 L2 AND WOOD T.3 => s solid feedstock 1369971 SOLID 26959 FEEDSTOCK L483 SOLID FEEDSTOCK (SOLID(W) FEEDSTOCK) \Rightarrow s 14 and 12 0 L4 AND L2 => s 14 and reformer 10533 REFORMER 0 L4 AND REFORMER 1.6 => s 14 and syngas 8553 SYNGAS L7 11 L4 AND SYNGAS => d 17 ibib abs 1-YOU HAVE REQUESTED DATA FROM 11 ANSWERS - CONTINUE? Y/(N):y ANSWER 1 OF 11 CAPLUS COPYRIGHT 2011 ACS on STN ACCESSION NUMBER: 2011:879941 CAPLUS DOCUMENT NUMBER: 155:157304 Systems and method for heating and drying solid TITLE: feedstock in a gasification system INVENTOR(S): Russell, Steven Craig; Corry, Judeth Brannon PATENT ASSIGNEE(S): General Electric Company, USA PCT Int. Appl., 33pp. SOURCE: CODEN: PIXXD2 DOCUMENT TYPE: Patent LANGUAGE: English FAMILY ACC. NUM. COUNT: 2 PATENT INFORMATION: KIND DATE APPLICATION NO. DATE PATENT NO. A2 20110714 WO 2011-US20354 20110106 WO 2011085087 W: AE, AG, AL, AM, AO, AT, AU, AZ, BA, BB, BG, BH, BR, BW, BY, BZ, CA, CH, CL, CN, CO, CR, CU, CZ, DE, DK, DM, DO, DZ, EC, EE, EG, ES, FI, GB, GD, GE, GH, GM, GT, HN, HR, HU, ID, IL, IN, IS, JP, KE, KG, KM, KN, KP, KR, KZ, LA, LC, LK, LR, LS, LT, LU, LY, MA, MD, ME, MG, MK, MN, MW, MX, MY, MZ, NA, NG, NI, NO, NZ, OM, PE, PG, PH, PL, PT, RO, RS, RU, SC, SD, SE, SG, SK, SL, SM, ST, SV, SY, TH, TJ, TM, TN, TR, TT, TZ, UA, UG, US, UZ, VC, VN, ZA, ZM, ZW RW: AL, AT, BE, BG, CH, CY, CZ, DE, DK, EE, ES, FI, FR, GB, GR, HR, HU, IE, IS, IT, LT, LU, LV, MC, MK, MT, NL, NO, PL, PT, RO, RS, SE, SI, SK, SM, TR, BF, BJ, CF, CG, CI, CM, GA, GN, GQ, GW, ML, MR, NE, SN, TD, TG, BW, GH, GM, KE, LR, LS, MW, MZ, NA, SD, SL, SZ, TZ, UG, ZM, ZW, AM, AZ, BY, KG, KZ, MD, RU, TJ, TM A1 20110707 US 2010-652835 20100106 US 2010-652835 A 20100106 US 20110162277 PRIORITY APPLN. INFO.: ASSIGNMENT HISTORY FOR US PATENT AVAILABLE IN LSUS DISPLAY FORMAT

AB A system for heating and drying a quantity of coal feedstock being channeled to a gasifier includes a first heat exchanger coupled in flow communication with the gasifier for transferring heat from an input stream to an output stream of heat transfer fluid, and a second heat exchanger positioned downstream from the first heat exchanger for receiving the

output stream of heat transfer fluid from the first heat exchanger, said second heat exchanger transfers heat from the output stream of heat transfer fluid to a stream of heating gas.

L7 ANSWER 2 OF 11 CAPLUS COPYRIGHT 2011 ACS on STN

ACCESSION NUMBER: 2011:849231 CAPLUS

DOCUMENT NUMBER: 155:157303

TITLE: Systems and method for heating and drying solid

feedstock in a gasification system

INVENTOR(S): Russell, Steven Craig; Corry, Judeth Brannon

PATENT ASSIGNEE(S): General Electric Company, USA SOURCE: U.S. Pat. Appl. Publ., 16pp.

CODEN: USXXCO

DOCUMENT TYPE: Patent LANGUAGE: English

FAMILY ACC. NUM. COUNT: 2

PATENT INFORMATION:

PAT					KIND I		DATE			APPLICATION NO.				DATE				
								US 2010-652835										
WO	WO 2011085087			A2 20110714			WO 2011-US20354				20110106							
	W:	ΑE,	ΑG,	AL,	ΑM,	ΑO,	ΑT,	ΑU,	ΑZ,	ΒA,	BB,	ΒG,	BH,	BR,	BW,	BY,	ΒZ,	
		CA,	CH,	CL,	CN,	CO,	CR,	CU,	CZ,	DE,	DK,	DM,	DO,	DZ,	EC,	EE,	EG,	
		ES,	FΙ,	GB,	GD,	GE,	GH,	GM,	GT,	HN,	HR,	HU,	ID,	IL,	IN,	IS,	JP,	
		ΚE,	KG,	KM,	KN,	ΚP,	KR,	KΖ,	LA,	LC,	LK,	LR,	LS,	LT,	LU,	LY,	MA,	
		MD,	ME,	MG,	MK,	MN,	MW,	MX,	MY,	MZ,	NA,	NG,	NΙ,	NO,	NZ,	OM,	PE,	
		PG,	PH,	PL,	PT,	RO,	RS,	RU,	SC,	SD,	SE,	SG,	SK,	SL,	SM,	ST,	SV,	
		SY,	TH,	ΤJ,	TM,	TN,	TR,	TT,	TZ,	UA,	UG,	US,	UZ,	VC,	VN,	ZA,	ZM,	ZW
	RW:	AL,	ΑT,	BE,	BG,	CH,	CY,	CZ,	DE,	DK,	EE,	ES,	FI,	FR,	GB,	GR,	HR,	
		ΗU,	ΙE,	IS,	ΙΤ,	LT,	LU,	LV,	MC,	MK,	MT,	NL,	NO,	PL,	PT,	RO,	RS,	
		SE,	SI,	SK,	SM,	TR,	BF,	ВJ,	CF,	CG,	CI,	CM,	GΑ,	GN,	GQ,	GW,	ML,	
		MR,	NE,	SN,	TD,	ΤG,	BW,	GH,	GM,	ΚE,	LR,	LS,	MW,	MZ,	NA,	SD,	SL,	
		SZ,	TZ,	UG,	ZM,	ZW,	ΑM,	AZ,	BY,	KG,	KΖ,	MD,	RU,	ΤJ,	TM			
PRIORITY APPLN. INFO.: US 2010-652835 A 20100106																		
ASSIGNMENT HISTORY FOR US PATENT AVAILABLE IN LSUS DISPLAY FORMAT																		

AB A system for heating and drying a quantity of coal feedstock being channeled to a gasifier includes a first heat exchanger coupled in flow communication with the gasifier for transferring heat from an input stream to an output stream of heat transfer fluid, and a second heat exchanger positioned downstream from the first heat exchanger for receiving the output stream of heat transfer fluid from the first heat exchanger, said second heat exchanger transfers heat from the output stream of heat transfer fluid to a stream of heating gas.

L7 ANSWER 3 OF 11 CAPLUS COPYRIGHT 2011 ACS on STN

ACCESSION NUMBER: 2011:815638 CAPLUS

DOCUMENT NUMBER: 155:129681

TITLE: Methods and apparatus for drying and gasification of

biomass

INVENTOR(S): Winter, John D.; Jacks, Curtis J.; Tirmizi, Shakeel H.

PATENT ASSIGNEE(S): Range Fuels, Inc., USA

SOURCE: U.S. Pat. Appl. Publ., 9pp.

CODEN: USXXCO

DOCUMENT TYPE: Patent LANGUAGE: English

FAMILY ACC. NUM. COUNT: 1

PATENT INFORMATION:

PATENT NO. KIND DATE APPLICATION NO. DATE

US 20110155958 A1 20110630 US 2010-980317 20101228 PRIORITY APPLN. INFO.: US 2009-291484P P 20091231 US 2009-291502P P 20091231

ASSIGNMENT HISTORY FOR US PATENT AVAILABLE IN LSUS DISPLAY FORMAT

AB In some variations, this invention provides a method of drying and gasifying a C-containing feedstock, comprising combusting methane to generate heat and a flue gas; drying the C-containing feedstock using part of the flue gas; and gasifying the dried feedstock to generate syngas. Some embodiments provide an apparatus for drying comprising a vessel; a primary channel for flowing the solid feedstock and a gas for drying the solid feedstock; a secondary channel for flowing the gas; and a plurality of internal screens or sieve plates suitable for passage of the gas. Other variations provide an apparatus including a primary vessel having a channel for axially flowing the solid feedstock; a pipe contained within the primary vessel, with a plurality of openings for radially distributing a gas for drying the solid feedstock; and a plurality of

exit ports at the walls for removal of the gas from the primary vessel.

L7 ANSWER 4 OF 11 CAPLUS COPYRIGHT 2011 ACS on STN

ACCESSION NUMBER: 2011:252161 CAPLUS

DOCUMENT NUMBER: 154:439671

TITLE: Evaluation of power generation schemes based on

hydrogen-fueled combined cycle with carbon capture and

storage (CCS)

AUTHOR(S): Cormos, Calin-Cristian

CORPORATE SOURCE: Faculty of Chemistry and Chemical Engineering,

Babes-Bolyai University, Cluj-Napoca, RO-400028, Rom.

SOURCE: International Journal of Hydrogen Energy (2011),

36(5), 3726-3738

CODEN: IJHEDX; ISSN: 0360-3199

PUBLISHER: Elsevier Ltd.

DOCUMENT TYPE: Journal LANGUAGE: English

IGCC is a power generation technol. in which the solid feedstock is partially oxidized to produce syngas. In a modified IGCC design for carbon capture, there are several technol. options which are evaluated in this paper. The first two options involve pre-combustion arrangements in which syngas is processed, either by shift conversion or chemical looping, to maximize the hydrogen level and to concentrate the carbon species as CO2. After CO2 capture by gas-liquid absorption or chemical looping, the hydrogen-rich gas is used for power generation. The third capture option is based on post-combustion arrangement using chemical absorption. Investigated coal-based IGCC case studies produce 400-500 MW net power with >90% carbon capture rate. Principal focus of the paper is concentrated on evaluation of key performance indicators for investigated carbon capture options, the influence of various gasifiers on carbon capture process, optimization of energy efficiency by heat and power integration, quality specification of captured CO2. The capture option with minimal energy penalty is based on chemical looping, followed by pre-combustion and post-combustion.

REFERENCE COUNT: 50 THERE ARE 50 CITED REFERENCES AVAILABLE FOR THIS RECORD. ALL CITATIONS AVAILABLE IN THE RE FORMAT

L7 ANSWER 5 OF 11 CAPLUS COPYRIGHT 2011 ACS on STN

ACCESSION NUMBER: 2011:96839 CAPLUS

TITLE: Design of a high temperature chamber fed by a plasma

torch for thermal removal of tars

AUTHOR(S): Fourcault, Alice; Marias, Frederic; Michon, Ulysse

CORPORATE SOURCE: Europlasma, Bordeaux, 33520, Fr.

SOURCE: Annual North American Waste to Energy Conference, Proceedings, 17th, Chantilly, VA, United States, May

18-20, 2009 (2009), 195-203. American Society of

Mechanical Engineers: New York, N. Y. CODEN: 69NRPW; ISBN: 978-0-7918-4880-7

DOCUMENT TYPE: Conference LANGUAGE: English

AB Biomass is one of the most important sources of renewable energy. One aim of Biomass gasification is to convert a solid feedstock into a valuable syngas for electricity or liquid fuel production Actual industrial auto-thermal gasification processes achieve a production of syngas mainly polluted by products such as dust, nitrogen oxides, sulfur dioxide and tars. Tars remain, one of the main drawbacks in using the gasification process since they are capable of condensing at low temperature. This could

lead

to fouling, corrosion, attrition and abrasion of downstream devices such as gas turbines or engines. Tars are often removed from the syngas, decreasing the internal energy of the syngas itself. These tars are heavy aromatic hydrocarbons whose treatment remains difficult by thermal, catalytic or even phys. methods. They can condense or polymerize into more complex structures, and the mechanisms responsible for their degradation are not completely identified and understood. Turboplasma is a thermal process, proposed by Europlasma. The main principle of operation relies on the use of thermal plasma for the cracking of tars inside a syngas produced in an auto-thermal gasification step. Basically, it consists of a degradation chamber where the syngas is heated by a plasma torch. The plasma plume provides a high temperature gas (around 5000K) to the system and enables heating of the incoming stream (above 1300K) and also generates high temperature zones (above 1600K) inside the device. Due to both high temperature

and long residence times of the syngas in the vessel, cracking of the tars occurs. Finally, the species released are mainly CO and H2, leading to an increase in the Lower Heating Value of the syngas. The work presented here describes the design of a high temperature gasification system assisted by thermal plasma. It was performed using a CFD computation implemented with a full chemical model for the thermal degradation of tars.

The

objectives were to understand the aerodynamic behavior of the vessel and to propose enhancement in its design. We present here some results of this study.

REFERENCE COUNT: 17 THERE ARE 17 CITED REFERENCES AVAILABLE FOR THIS RECORD. ALL CITATIONS AVAILABLE IN THE RE FORMAT

L7 ANSWER 6 OF 11 CAPLUS COPYRIGHT 2011 ACS on STN

ACCESSION NUMBER: 2010:1566374 CAPLUS

DOCUMENT NUMBER: 154:32413

TITLE: Method of using syngas cooling to heat drying gas

for a dry feed system

INVENTOR(S): Russell, Steven Craig; Corry, Judeth Brannon; Frey,

Geroge Frederick; Mishra, Sunil Ramabhilakh; Mall,

Omprakash

PATENT ASSIGNEE(S): USA

SOURCE: U.S. Pat. Appl. Publ., 20pp.

CODEN: USXXCO

DOCUMENT TYPE: Patent LANGUAGE: English

FAMILY ACC. NUM. COUNT: 1

PATENT INFORMATION:

PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
US 20100313442 CA 2705645	A1 A1	20101216 20101212	US 2009-483314 CA 2010-2705645	20090612 20100527

AU 2010202283 A1 20110106 AU 2010-202283 20100602 CN 101922851 A 20101222 CN 2010-10208550 20100611 PRIORITY APPLN. INFO.: US 2009-483314 A 20090612

ASSIGNMENT HISTORY FOR US PATENT AVAILABLE IN LSUS DISPLAY FORMAT

AB A method for improving the overall thermal efficiency of a coal power generation plant by transferring heat from a raw synthesis gas stream to solid fuel used as the primary feed to the gasifier, comprising the steps of initially cooling the syngas exhaust by transferring heat to a makeup conveyance gas feed to the dry feed preparation system, feeding a solid fuel component and a portion of the makeup gas stream into a grinding mechanism for the solid feedstock, forming a two-phase solids/gas stream comprising ground feedstock particulates and makeup gas, heating and drying the ground solid feedstock particulates to remove water, separating and removing water vapor formed in the heating and drying step, and feeding the heated and dried solids/gas stream to the gasifier.

L7 ANSWER 7 OF 11 CAPLUS COPYRIGHT 2011 ACS on STN

ACCESSION NUMBER: 2010:1105889 CAPLUS

DOCUMENT NUMBER: 153:534294

TITLE: Mathematical modeling and simulation of gasification

processes with carbon capture and storage (CCS) for

energy vectors poly-generation

AUTHOR(S): Maxim, Victoria; Cormos, Calin-Cristian; Cormos,

Ana-Maria; Agachi, Serban

CORPORATE SOURCE: Faculty of Chemistry and Chemical Engineering, Babes -

Bolyai University, Cluj - Napoca, RO-400028, Rom. Computer-Aided Chemical Engineering (2010), 28(20th

European Symposium on Computer Aided Process

Engineering, 2010), 697-702

CODEN: CACEFH

PUBLISHER: Elsevier B.V.

DOCUMENT TYPE: Journal LANGUAGE: English

SOURCE:

Gasification of solid fuels is a partial oxidation process which converse the AΒ solid feedstock into syngas which can be used in a large number of applications e.g. power generation, manufacture of various chems. and fuels (hydrogen, methanol, ammonia, fertilizers etc.). Not all of the gasification systems are suitable for energy vectors poly-generation with carbon capture and storage (CCS). This paper is proposing to evaluate various gasification technologies by math. modeling and simulation methods (especially for entrained flow types as these gasifiers are more suitable for implementing carbon capture technologies). In this paper a particular accent will be put on the selection of the most promising gasifier, as not all are appropriate for a carbon capture Integrated Gasification Combined Cycle (IGCC) applied for energy vectors poly-generation (with a particular focus on hydrogen and electricity co-production case) with Carbon Capture and Storage (CCS). For the selection of the most appropriate gasifier technologies the process were math. modeled and simulated with process flow modeling software (e.g. ChemCAD, Aspen). In the evaluation of various gasification technologies (e.g. Shell, Siemens, GE-Texaco, Conoco-Phillips etc.) a multi-criteria anal. was performed.

OS.CITING REF COUNT: 1 THERE ARE 1 CAPLUS RECORDS THAT CITE THIS RECORD

(1 CITINGS)

REFERENCE COUNT: 9 THERE ARE 9 CITED REFERENCES AVAILABLE FOR THIS RECORD. ALL CITATIONS AVAILABLE IN THE RE FORMAT

L7 ANSWER 8 OF 11 CAPLUS COPYRIGHT 2011 ACS on STN

ACCESSION NUMBER: 2010:841312 CAPLUS

DOCUMENT NUMBER: 153:338438

TITLE: Evaluation of energy integration aspects for

IGCC-based hydrogen and electricity co-production with

carbon capture and storage

AUTHOR(S): Cormos, Calin-Cristian

CORPORATE SOURCE: Faculty of Chemistry and Chemical Engineering, Babes -

Bolyai University, Cluj - Napoca, RO-400028, Rom.
International Journal of Hydrogen Energy (2010)

SOURCE: International Journal of Hydrogen Energy (2010),

35(14), 7485-7497

CODEN: IJHEDX; ISSN: 0360-3199

PUBLISHER: Elsevier Ltd.

DOCUMENT TYPE: Journal; General Review

LANGUAGE: English

A review. Integrated Gasification Combined Cycle (IGCC) is a power generation technol. in which the solid feedstock is partially oxidized with oxygen and steam to produce syngas. In a conventional IGCC design without carbon capture, the syngas is purified for dust and hydrogen sulfide removal and then sent to a Combined Cycle Gas Turbine (CCGT) for power generation. Carbon capture technologies are expected to play an important role in the coming decades for reducing the greenhouse gas emissions. In a modified IGCC design for carbon capture, the syngas is catalytically shifted to maximize the hydrogen level and to concentrate the carbon species in the form of carbon dioxide which can be later captured in a pre-combustion arrangement. After carbon dioxide capture, the hydrogen-rich syngas can be either purified in a Pressure Swing Adsorption (PSA) unit and exported to the external customers (e.g., chemical industry, PEM fuel cells) or used in a CCGT for power generation. paper investigates the most important energy and process integration issues for hydrogen and electricity co-production scheme based on coal gasification process with carbon capture and storage (CCS). The evaluated coal-based IGCC case produces around 400 MW net electricity and has a flexible hydrogen output in the range of 0-200 MW (LHV) with a 90% carbon capture rate. The principal focus of the paper is on the evaluation of energy integration aspects so as to maximize the overall plant energy efficiency. Optimization includes heat and power integration of the main plant sub-systems (e.g., integration of steam generated in gasification island, with the requirements for syngas treatment, power generation in the combined cycle, best use of PSA tail gas in the power block, heat and power demand for acid gas removal unit, integration of air separation unit and gas turbine compressor etc.), sensitivity anal. (e.g., influence on ambient conditions).

OS.CITING REF COUNT: 3 THERE ARE 3 CAPLUS RECORDS THAT CITE THIS RECORD

(3 CITINGS)

REFERENCE COUNT: 43 THERE ARE 43 CITED REFERENCES AVAILABLE FOR THIS RECORD. ALL CITATIONS AVAILABLE IN THE RE FORMAT

L7 ANSWER 9 OF 11 CAPLUS COPYRIGHT 2011 ACS on STN

ACCESSION NUMBER: 2009:1317033 CAPLUS

DOCUMENT NUMBER: 153:647381

TITLE: Conversion of syngas from biomass in solid oxide

fuel cells

AUTHOR(S): Karl, Jurgen; Frank, Nadine; Karellas, Sotirios;

Saule, Mathilde; Hohenwarter, Ulrich

CORPORATE SOURCE: Institute of Thermal Engineering, Technical University

of Graz, A 8010 Graz, Austria

SOURCE: Journal of Fuel Cell Science and Technology (2009),

6(2), 021005/1-021005/6

CODEN: JFCSAU; ISSN: 1550-624X

PUBLISHER: American Society of Mechanical Engineers

DOCUMENT TYPE: Journal LANGUAGE: English

AB Conversion of biomass in syngas by means of indirect gasification offers the option to improve the economic situation of any fuel cell system due to lower costs for feedstock and higher power revenues in many European

countries. The coupling of an indirect gasification of biomass and residues with highly efficient solid oxide fuel cell (SOFC) systems is therefore a promising technol. for reaching economic feasibility of small decentralized combined heat and power production (CHP). The predicted efficiency of common high temperature fuel cell systems with integrated gasification of solid feedstock is usually significantly lower than the efficiency of fuel cells operated with hydrogen or methane. Addnl. system components like the gasifier as well as the gas cleaning reduce this efficiency. Hence common fuel cell systems with integrated gasification of biomass will hardly reach elec. efficiencies above 30%. An extraordinary efficient combination is achieved in case that the fuel cells waste heat is used in an indirect gasification system. A simple combination of a SOFC and an allothermal gasifier enables then elec. efficiencies above 50%. However, this system requires an innovative cooling concept for the fuel cell stack. Another significant question is the influence of impurities on the fuel cell degradation The European Research Project "BioCellus" focuses on both questions-the influence of the biogenous syngas on the fuel cells and an innovative cooling concept based on liquid metal heat pipes. First expts. showed that, in particular, higher hydrocarbons-the so-called tars-do not have any significant influence on the performance of SOFC membranes. The innovative concept of the TopCycle comprises to heat an indirect gasifier with the exhaust heat of the fuel cell by means of liquid metal heat-pipes. Internal cooling of the stack and the recirculation of waste heat increases the system efficiency significantly. This concept promises elec. efficiencies of above 50% even for small-scale systems without any combined processes.

REFERENCE COUNT: 12 THERE ARE 12 CITED REFERENCES AVAILABLE FOR THIS RECORD. ALL CITATIONS AVAILABLE IN THE RE FORMAT

L7 ANSWER 10 OF 11 CAPLUS COPYRIGHT 2011 ACS on STN

ACCESSION NUMBER: 2009:899816 CAPLUS

DOCUMENT NUMBER: 153:41381

AUTHOR(S):

TITLE: Assessment of hydrogen and electricity co-production

schemes based on gasification process with carbon

capture and storage Cormos, Calin-Cristian

CORPORATE SOURCE: Faculty of Chemistry and Chemical Engineering,

Babes-Bolyai University, Cluj-Napoca, 400028, Rom.

SOURCE: International Journal of Hydrogen Energy (2009),

34(15), 6065-6077

CODEN: IJHEDX; ISSN: 0360-3199

PUBLISHER: Elsevier Ltd.

DOCUMENT TYPE: Journal LANGUAGE: English

Through gasification, a solid feedstock is partially oxidized with AB oxygen and steam to produce syngas which can be used for conversion into different valuable compds. (e.g. hydrogen) or to generate power in a combined cycle gas turbine (CCGT). Integrated gasification combined cycle (IGCC) is one of power generation technologies having the highest potential for carbon capture with low penalties in efficiency and cost. This paper assesses from tech. point of view the transformation, through gasification, of coal with or without addition of renewable energy sources or solid waste into decarbonised energy vectors (power, hydrogen) simultaneous with carbon capture and storage (CCS). Investigated plant concepts produce a flexible ratio of power and hydrogen in the range of 400~MW electricity and 0--200~MW hydrogen with 90% carbon capture rate. The paper describes the methodol. to evaluate the plant performances using critical design factors like: fuel selection criteria, choice of gasification reactor, heat and power integration, flexibility anal., carbon capture and storage (CCS), H2 and CO2 quality specifications considering the use of hydrogen in transport sector (fuel cells) and carbon dioxide storage in

geol. formation or using for Enhanced Oil Recovery (EOR).

OS.CITING REF COUNT: 17 THERE ARE 17 CAPLUS RECORDS THAT CITE THIS

RECORD (17 CITINGS)

39 THERE ARE 39 CITED REFERENCES AVAILABLE FOR THIS REFERENCE COUNT: RECORD. ALL CITATIONS AVAILABLE IN THE RE FORMAT

ANSWER 11 OF 11 CAPLUS COPYRIGHT 2011 ACS on STN L7

2007:280133 CAPLUS ACCESSION NUMBER:

DOCUMENT NUMBER: 148:475584

TITLE: Conversion of syngas from biomass in solid oxide

fuel cells

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Conversion of biomass in syngas by means of indirect gasification offers the option to improve the economic situation of any fuel cell systems due to lower costs for feedstock and higher power revenues in many European countries. The coupling of an indirect gasification of biomass and residues with highly efficient SOFC systems is therefore a promising technol. for reaching economic feasibility of small decentralized combined heat and power production (CHP). The predicted efficiency of common high temperature fuel cell systems with integrated gasification of solid feedstock is usually significantly lower than the efficiency of fuel cells operated with H or methane. Addnl. system components like the gasifier, as well as the gas cleaning reduce this efficiency. Hence, common fuel cell systems with integrated gasification of biomass will hardly reach elec. efficiencies >30%. An extraordinary efficient combination is achieved in case that the fuel cells waste heat is used in an indirect gasification system. A simple combination of a SOFC and an allothermal gasifier enables then elec. efficiencies >50%. But this systems requires an innovative cooling concept for the fuel cell stack. Another significant question is the effect of impurities on the fuel cells degradation The European Research Project BioCellus focuses on both questions, the effect of the biogenous syngas on the fuel cells and an innovative cooling concept based on liquid metal heat pipes. First expts. showed that in particular higher hydrocarbons, the so-called tars, do not have an significant effect on the performance of SOFC membranes. The innovative concept of the TopCycle comprises to heat an indirect gasifier with the exhaust heat of the fuel cell by liquid metal heat pipes. Internal cooling of the stack and the recirculation of waste heat increases the system efficiency significantly. This concept promises elec. efficiencies of >50% even for small-scale systems without any combined processes.

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